

[0068] Although FIGS. 4-8 depict essentially vertical flow through the channels, these distillation units may be aligned horizontally to provide for horizontal flow through the channels, or they may be aligned at an inclined angle from the horizontal.

[0069] An alternate embodiment of the microchannel condenser 120 illustrated in FIGS. 1 and 2 and the microchannel condenser 120B illustrated in FIG. 8 is disclosed in FIGS. 9-11. Referring to FIGS. 9-11, microchannel condenser 500 comprises process microchannel 510, liquid channels 520 and 530, heat exchange channels 540 and 550, and outlet 560. Liquid channel 520 includes wicking region 525 and outlet 527, and liquid channel 530 includes wicking region 535 and outlet 537. Process microchannel 510 is positioned between liquid channels 520 and 530. Heat exchange channels 540 are adjacent to liquid channel 520. Heat exchange channels 550 are adjacent to liquid channel 530. Process microchannel 510 includes inlet 511 for permitting vapor to flow into the process microchannel 510, and outlets 512 and 514 for permitting condensed vapor to flow from process microchannel 510 into wicking regions 525 and 535, respectively. In operation, vapor 518 flows through inlet 517 into process microchannel 510 in the direction indicated by arrow 516 and condenses to form condensed vapor 519 which may be referred to as distillation product D. Heat exchange fluid flows through heat exchange channels 540 and 550 in a direction that is crosscurrent relative to the flow of vapor in the process microchannel 510. Part or all of the condensed vapor may flow through outlet 560, as indicated by arrow 562. The remaining condensed vapor may flow through outlets 512 and 514 into wicking regions 525 and 535, respectively. The distillate product flowing in the wicking regions 525 and 535 flows in the direction indicated by arrows 526 and 536 through outlets 527 and 537, respectively.

[0070] An alternate embodiment of the microchannel reboiler 130 illustrated in FIGS. 1 and 2 and the microchannel reboiler 130B illustrated in FIG. 8 is disclosed in FIGS. 12-14. Referring to FIGS. 12-14, microchannel reboiler 600 comprises process microchannel 610, liquid channel 620, and heat exchange channels 630 and 640. Liquid channel 620 includes wicking region 625. Process microchannel 610 is positioned between liquid channel 620 and heat exchange channels 630. Heat exchange channels 640 are adjacent to liquid channel 620. Process microchannel 610 includes outlets 612 and 614, and inlet 616. In operation, liquid 619 flows through wicking region 625 to inlet 616, and through inlet 616 into process microchannel 610, as indicated by arrow 626. Heat exchange fluid flows through heat exchange channels 630 and 640 in a direction that is crosscurrent relative to the flow of liquid through the wicking region 625. Part or all of the liquid 619, which is in the form of bottoms product B, may flow through outlet 612, as indicated by arrow 613. The remainder of the bottoms product B may be vaporized. The vapor 618 flows through process microchannel 610 in the direction indicated by arrow 615 and out of process microchannel 610 through outlet 614.

[0071] An alternate embodiment of the microchannel reboiler 130 illustrated in FIGS. 1 and 2 and the microchannel reboiler 130B illustrated in FIG. 8 is disclosed in FIGS. 15-17. Referring to FIGS. 15-17, microchannel reboiler 700 comprises process microchannel 710, liquid

channel 720, and heat exchange channels 730 and 740. Liquid channel 720 includes wicking region 725. Process microchannel 710 is positioned between liquid channel 720 and heat exchange channels 730. Heat exchange channels 740 are adjacent to liquid channel 720. Process microchannel 710 includes outlets 712 and 714, and inlet 716. In operation, liquid 719 flows through wicking region 725 to inlet 716, and through inlet 716 into process microchannel 710, as indicated by arrow 726. Heat exchange fluid flows through heat exchange channels 730 and 740 in a direction that is crosscurrent relative to the flow of liquid through the wicking region 725. Part or all of the liquid 719, which is in the form of bottoms product B, may flow through outlet 712, as indicated by arrow 713. The remainder of the bottoms product B may be vaporized. The vapor 718 flows through process microchannel 710 in the direction indicated by arrow 715 and out of process microchannel 710 through outlet 714.

[0072] The microchannel condenser (120, 120B, 500) and microchannel reboiler (130, 130B, 600, 700) as components of the inventive microchannel distillation unit (300, 300A, 300B, 400) can be integrated into the manifolds (header and footer) of the process microchannels (310, 420, 425, 420a, 425a) and liquid channels (330, 415). An example of manifolding with an integrated microchannel reboiler is shown in FIGS. 12-14. The liquid from the last section of the liquid channel (stream 336 in FIG. 8) flows into the footer/reboiler section at the unit end and is heated by the heat exchange channels 630 and 640. Vapor is formed and flows upwards, as indicated by arrow 615, back into the process channels via buoyancy. Part of the liquid is drained through the common outlet 612 at the bottom as the bottoms product so that a splitting of boil-up ratio can be controlled by the flow conditions and configuration of the microchannel reboiler. Another example is illustrated in FIGS. 15-17 where the common outlet of the process channels' footer is located at the side. To prevent carryover of the vapor by the liquid to be drained as product, an extruded edge may be made at the end of each horizontal separation wall. As the heat transfer area is different from channel to channel in a single layer of the unit, the duty of the reboiler microchannel may have to be different. For example, the duty in heat exchange channel 740A may have to be higher than in channel 740B, as horizontal channel 740A is shorter than 740B. Control of the duty in an individual microchannel reboiler heat exchange channel can be made by changing flow rate, inlet temperature and/or pressure.

[0073] The manifold (header) may be located at the end of the unit (FIGS. 9-11) where vapor is cooled and partly condensed by the integrated microchannel condenser. The condensation occurs on the wicking structure surface as heat is removed from the wick by the integrated condenser. The condensate may be enriched in the less volatile component and is sucked in by the wicking structure and transported along the liquid channel. The uncondensed vapor leaves the outlet of the manifold so that a reflux is realized. The reflux ratio can be controlled by controlling the duty of the microchannel condenser.

[0074] The microchannel distillation unit 300C illustrated in FIG. 18 is a slightly modified version of the microchannel distillation unit 300A illustrated in FIG. 5. The microchannel distillation unit 300C contains a plurality of adjacent distillation units 302 arranged in parallel spaced rows 303.